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Dynamics of bubble population undergoing mass transfer and coalescence in a glass forming liquid

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1. Problem statement



Figure 1: Binarized optical microscope images¹.

¹L. Pereira et al.: Experimental study of bubble formation in a glass-forming liquid doped with cerium oxide, in: J. Am. Ceram. Soc. 103 (2020), pp. 2453–2462.

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Figure 2: Bubble density vs. t obtained expérimentally at T=1100 °C.



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According to Cable²:

Coalescence is obviously an important phenomenon during the early stages of melting but the conditions favourable to the coalescence of bubbles have been little investigated.

²M. Cable: A study of refining. Part 2: Mechanisms of refining, in: Glass Technol. 2 (1961), pp. 60–70.

- 1. Problem statement
- 2. Population balance equation
- 3. Direct quadrature method of moments
- 4. Numerical results
- 5. Synthesis & perspectives



4

The conservation of the PDF is given by the Liouville equation³:

$$\frac{\partial f}{\partial t} + \boldsymbol{\nabla} \cdot (\mathbf{v}f) + \frac{\partial (\dot{a}f)}{\partial a} + \sum_{i=1}^{N_g - 1} \frac{\partial (\dot{\mathbf{x}}_{g,i}f)}{\partial \mathbf{x}_{g,i}} = h(\mathbf{x}, t; a, \mathbf{x}_g), \tag{1}$$

³D. Ramkrishna: Population balances. Theory and application to particulate systems in engineering, San Diego 2000.

⁴F. Pigeonneau: Mechanism of mass transfer between a bubble initially composed of oxygen and molten glass, in: Int. J. Heat Mass Transfer 54 (2011), pp. 1448–1455.

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with⁴

$$\mathbf{v} = \mathbf{u} - \frac{\mathbf{g}a^2}{3\nu},\tag{2}$$

$$\dot{a} = \frac{1}{2a} \sum_{i=1}^{N_g} \operatorname{Sh}(\operatorname{Pe}_i) \mathcal{H}_i \mathcal{D}_i \left(\mathbf{x}_{l,i} - \mathbf{x}_{g,i} \right), \ \mathcal{H}_i = \mathcal{L}_i RT, \ \mathbf{x}_{l,i} = \frac{C_{l,i}}{\mathcal{L}_i P}, \quad (3)$$

$$\dot{\mathbf{x}}_{g,i} = \frac{3}{2a^2} \sum_{j=1}^{N_g} \mathrm{Sh}(\mathrm{Pe}_j) \mathcal{H}_j \mathcal{D}_j \left(\delta_{ij} - \mathbf{x}_{g,i} \right) \left(\mathbf{x}_{l,j} - \mathbf{x}_{g,j} \right), \forall i = [1; N_g - 1](4)$$

³Ramkrishna: Population balances. Theory and application to particulate systems in engineering (see n. 3).

⁴Pigeonneau: Mechanism of mass transfer between a bubble initially composed of oxygen and molten glass (see n. 4).

To solve the PBE, a size-conditioned density is defined⁵:

$$n(\mathbf{x}, t; \mathbf{a}) = \int_{\Omega_{\mathbf{x}_g}} f(\mathbf{x}, t; \mathbf{a}, \mathbf{x}_g) d\mathbf{x}_g,$$
 (5)

and a size-conditioned of a quantity G is

$$\langle G|a \rangle = rac{\int_{\Omega_{\mathbf{x}_g}} Gf(\mathbf{x}, t; a, \mathbf{x}_g) d\mathbf{x}_g}{n(\mathbf{x}, t; a)}.$$
 (6)

After volume average, the PBE becomes

$$\frac{\partial \langle n \rangle}{\partial t} + \frac{\partial (\langle \dot{a} | a \rangle \langle n \rangle)}{\partial a} = \langle S \rangle (t; a) - \frac{\langle n \rangle g a^2}{3\nu}.$$
 (7)

⁵D. L. Marchisio/R. O. Fox: Computational models for polydisperse particulate and multiphase systems, 2013.

• The coalescence source term, $S(\mathbf{x}, t; a)$, is given by⁶

$$\langle S \rangle(t;a) = \frac{1}{2} \int_{0}^{a} \frac{a^{2}}{(a^{3} - a'^{3})^{2/3}} K\left(a', \sqrt[3]{a^{3} - a'^{3}}\right) \langle n \rangle(t;a') \langle n \rangle\left(t;\sqrt[3]{a^{3} - a'^{3}}\right) da' - \langle n \rangle(t;a') \int_{0}^{\infty} K\left(a,a'\right) \langle n \rangle(t;a') da'.$$
(8)

Due to the bubble rising, the coalescence kernel can be written as follows⁷

$$K(a, a') = \frac{g\pi}{3\nu} (a + a')^2 |a^2 - a'^2| E_{col}(a, a').$$
(9)

⁶Marchisio/Fox: Computational models for polydisperse particulate and multiphase systems (see n. 5).

⁷X. Zhang/R. H. Davis: The rate of collisions due to Brownian or gravitational motion of small drops, in: J. Fluid Mech. 230 (1991), pp. 479–504.



Figure 3: Coalescence efficiency for gravity sedimentation⁸.

 $^{^{8}}$ Zhang/Davis: The rate of collisions due to Brownian or gravitational motion of small drops (see n. 7).



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Table 1: Characteristic quantities for the normalisation.

$$a \quad t \quad \mathbf{v} \quad \langle n \rangle$$

$$a_0 \quad \frac{3H\nu}{ga_0^2} \quad \frac{ga_0^2}{3\nu} \quad \frac{N_0}{a_0}$$

$$\varphi_0 = \frac{4\pi a_0^3 N_0}{3}.$$
(10)

$$K(a, a') = K_0 E_{coa} (a + a')^2 |a^2 - a'^2|, \qquad (11)$$
$$K_0 = \pi N_0 a_0^2 H. \qquad (12)$$





Figure 4: $\langle n \rangle$ vs. *a* and discrete representation of $\langle n \rangle$.

$$\langle n \rangle(t;a) = \sum_{\alpha=1}^{N} \omega_{\alpha}(t) \delta[a - a_{\alpha}(t)],$$
 (13)

 ω_{α} : weight, a_{α} : abscissa.



In direct method, equations are written in ω_{α} and a_{α}^9 :

$$\frac{d\omega_{\alpha}}{dt} = A_{\alpha}, \ \frac{d(\omega_{\alpha}a_{\alpha})}{dt} = B_{\alpha}, \ \forall \alpha \in [1, N],$$
(14)

$$(1-k)\sum_{\alpha=1}^{N} a_{\alpha}^{k} A_{\alpha} + k \sum_{\alpha=1}^{N} a_{\alpha}^{k-1} B_{\alpha} = C_{k}, \ \forall \ k \in [0; 2N-1],$$
(15)

$$C_{k} = \sum_{\alpha=1}^{N} \sum_{\beta=1}^{N} \omega_{\alpha} \omega_{\beta} K(\mathbf{a}_{\alpha}, \mathbf{a}_{\beta}) \left[\frac{\left(\mathbf{a}_{\alpha}^{3} + \mathbf{a}_{\beta}^{3} \right)^{k/3}}{2} - \mathbf{a}_{\beta}^{k} \right] + k \sum_{\alpha=1}^{N} \mathbf{a}_{\alpha}^{k-1} \langle \dot{\mathbf{a}} | \mathbf{a}_{\alpha} \rangle \omega_{\alpha}$$

$$-\sum_{\alpha=1}^{N}\omega_{\alpha}a_{\alpha}^{k+2},\tag{16}$$

$$rac{d\langle \mathrm{x}_{m{g},i}|m{a}_{lpha}
angle}{dt} = rac{3}{2m{a}_{lpha}^2}\sum_{j=1}^{N_{m{g}}}\mathrm{Sh}(\mathrm{Pe}_{j,lpha})\mathcal{H}_{j}\,\mathrm{Fo}_{j}\left(\delta_{ij}-\langle\mathrm{x}_{m{g},i}|m{a}_{lpha}
angle
ight)\left(\mathrm{x}_{l,j}-\langle\mathrm{x}_{m{g},j}|m{a}_{lpha}
angle
ight),$$

$$\forall i \in [1, N_g - 1], \tag{17}$$

$$\frac{d\mathbf{x}_{l,i}}{dt} = -\frac{3\varphi_0}{2} \sum_{\alpha=1}^{N} \mathbf{a}_{\alpha} \omega_{\alpha} \operatorname{Sh}(\operatorname{Pe}_{i,\alpha}) \operatorname{Fo}_i(\mathbf{x}_{l,i} - \langle \mathbf{x}_{g,i} | \mathbf{a}_{\alpha} \rangle), \ \forall i \in [1, N_g].$$
(18)

 9 Marchisio/Fox: Computational models for polydisperse particulate and multiphase systems (see n. 5).

1. Initialisation of 2N first moments μ_k from an initial pdf:

$$\mu_{k} = \int_{0}^{\infty} a^{k} \langle n \rangle (t; a) da = \sum_{\alpha=1}^{N} a_{\alpha}^{k} \omega_{\alpha}.$$
 (19)

- 2. Determine $(a_{\alpha}, \omega_{\alpha})$ from the 2*N* first moments using the Wheeler algorithm¹⁰;
- 3. Solve the ODE for ω_{α} , $\omega_{\alpha}a_{\alpha}$, $\langle \mathbf{x}_{g,i}|a_{\alpha}\rangle$ & $\mathbf{x}_{I,i}$ using a RK4.
- 4. Compute the 2*N* first μ_k .

¹⁰J. C. Wheeler: Modified moments and Gaussian quadratures, in: Rocky Mt. J. Math. 4.2 (1974), pp. 287–296.

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In numerical applications: N = 3.

¹⁰Wheeler: Modified moments and Gaussian quadratures (see n. 10).

Extraction from the 2D images¹¹, the 3D relevant data¹².

T (°C)	<i>N</i> ₀ (mm ^{−3})	$arphi_{0}$	<i>a</i> 0 (µm)	K_0
1000	345	$8.64 imes10^{-2}$	39.07	33.17
1050	190	$1.01 imes10^{-1}$	50.27	30.19
1100	68.8	$1.11 imes10^{-1}$	72.91	22.99

Table 2: Initial N_0 , φ_0 , $a_0 \& K_0$.

¹¹Pereira et al.: Experimental study of bubble formation in a glass-forming liquid doped with cerium oxide (see n. 1).

¹²A. Baddeley/E. B. Vedel Jensen: Stereology for statisticians, 2005.



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5. Synthesis & perspectives

 Gravity sedimentation kernel explained the coalescence in a crucible experiment.

Coalescence becomes important if

$$K_0 \sim 1 \rightarrow N_0 > 10^2 \text{ cm}^{-3}.$$
 (20)

- The probability of the coalescence $\sim 1/\sqrt[3]{N_0} \sim 1$ mm.
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5. Synthesis & perspectives

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- The probability of the coalescence $\sim 1/\sqrt[3]{N_0} \sim 1 \,\mathrm{mm}$.
- DQMOM is an efficient method to solve PBE.
- To be used in CFD software (Ansys Fluent).
- Need a coalescence kernel accounting for fluid motion.
- Introduce the redox & fining.



5. Synthesis & perspectives

Thank you for your attention!

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